† . *

Development of Performance Test Apparatus and Design Program of Liquid-Phase Plate Heat Exchanger

Sang-il Park and Young-Ho Song

Key Words: Plate Heat Exchanger(), Performance Test Apparatus()

Design Program(), Liquid-Phase()

Abstract

The performance test apparatus of liquid-phase plate heat exchanger was installed and the computer program for design was developed in this study. The detail temperature distribution of hot and cold fluids in each path of heat exchanger was calculated by numerical method and the correlation for the heat transfer coefficient was defined. The heat transfer coefficients were measured using the working fluids of water and glycerine to investigate the effect of fluid viscosity. The measured heat transfer coefficients were compared with the calculated values obtained from the computer program and it was shown that error of the calculated values was generally less than 5%.

Α Cp 1. : F-factor LMTD: 가 m Q T U ΛT 10% 가 가 c h E-mail: sipark@kier.re.kr TEL: (042)860-3313 FAX: (042)860-3102 가 가

가

2. 2-1. pass 5 pass 가 가 end effect chart DX-3, DX-22, DX-143 가 DX-146 chart database가 $m_h Cp_h (T_{hi} - T_{ho}) = UA (T_h - T_c)$ database $m_{c}Cp_{c}(T_{co}-T_{ci})=UA(T_{h}-T_{c})$ 2-2. 가 가 가 1 , end plate effect가 가 , end plate effect 40 가 pass 가 end plate effect 가 pass 가 5 가 가 80°C 가 가 20°C ${\tt program}$

program

 U_{avg}

 U_{cal}

2004

 U_{avg} U_{cal} 12 2가 $Q = \dot{m}_h Cp_h (T_{hi} - T_{ho})$ 4% F-factor $LMTD = \frac{(T_{hi} - T_{co}) - (T_{ho} - T_{ci})}{Ln((T_{hi} - T_{co})/(T_{ho} - T_{ci}))}$ F-factor $U_{cal} = Q/(LMTD \cdot A)$ $F = U_{cal} / U_{avg}$ U_{cal} U_{avg} 가 DX-22H 가 80°C 20°C 가 0.1kg/s U_{avg} U_{cal} F-factor Fig. 2 $\Delta T = F \cdot LMTD$ Fig. 2 가 1 F-factor 가 2 0.87 1.0 F factor 가 가 1.0 , F=1 가 5 end plate effect 2-3. F factor D 1.0 Fig. 1 가 80°C 20°C 가 5 $Nu = C Re^{X} Pr^{Y} (\mu_b/\mu_w)^{Z}$ program U_{cal} C, X, Z 0.0005 2.0 kg/s Pr 10000 1.05 F-factor or Ucal/Uav 6.0 6.0 68.0 1000 U (W/m2K) 100 10 U-cal U-avg 8.0 0.0001 1000

Fig. 2 Variation of F-factor

no. of flow path

Υ

Water flowrate(kg/s)

Fig. 1 Comparison of U_{cal} with U_{avg} when no. of

path is 5

3.	Conting Trans	
3-1.	PLANT DE SE SESSION	
2003 9 . Fig. 3		E .
DX-22	Total Rate O O PLAF	PLATE HEAT E-CRANGES
, ,	Fig. 3 Schematic of heat exchanapparatus	ger test
, , 가 .	3-2.	
datalogger PC , フト ,		가
6 10kW 가	1	
. 20RT ,	가	,
	,	
·	, 가	,
·	RTD	
. 2200mm x 1500mm x 2200mm . 1.5		
kW 4	datalogger ,	PC PC
,	,	
	가 100%가 d	, atalogger 4
3 RTD 5 RTD	·	7
. RTD 4-wire type , 3.2mm .	, ,	
· · · · · · · · · · · · · · · · · · ·	가	,

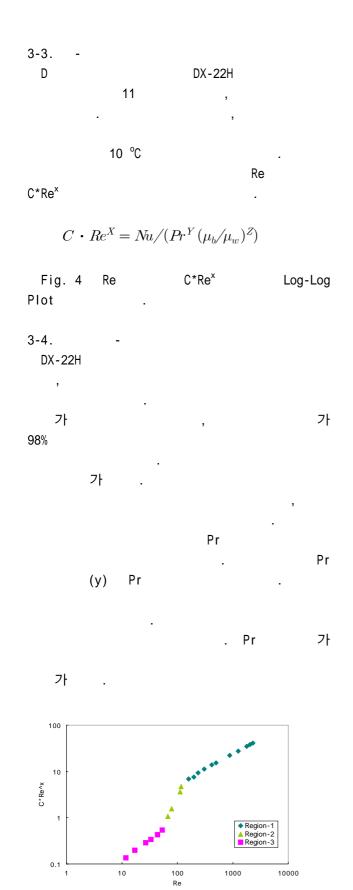


Fig. 4 Experimental results of DX-22H water-water heat exchanger

DX-22H - C*Re^x
- C*Re^x
Fig. 5 . Fig. 5 ,

Fig. 5

, Re

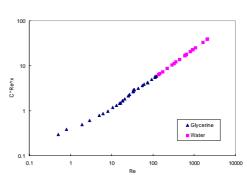


Fig. 5 Experimental results of DX-22H glycerine-water heat exchanger

Table 1 Values and errors of C*Re^x

Re	water -water	glycerine -water	Error (%)
121.6	5.891	5.835	-0.9
112	5.604	5.841	+4.2
111.5	5.561	5.517	-0.8
93.7	4.952	4.988	+0.7

2004

4.

DX-3, DX-22H, DX-22L, DX-143H, DX-143L DX-146H 6가 - DX-22H DX-143H 2가

Fig. 6

.

. Fig. 6 , 5% Re 가

2%

5.

가

5% .

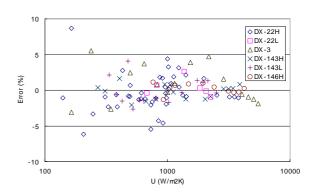


Fig. 6 Error of calculation results using design computer program

- (1) Park, S. I., 2004, "Technical Support for Development of Plate Heat Exchanger Test Apparatus and Design Program" KIER Report.
- (2) Min, E. D., 1995, Theory and Design of Heat Exchanger, Young-Poong Publ. co.
- (3) Touloukian, Y. S., Powell, R. W., Ho, C. Y. and Klemens, P. C., 1970, Thermal conductivity, IFI/Plenum, New York, Washington.