

Oxygen Sensitivity of Carbon Monoxide-Dependent Hydrogen Production Activity in *Citrobacter* sp.

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Abstract A newly isolated *Citrobacter* sp. Y19 catalyzes the CO-dependent H₂ production (biological water-gas shift reaction) by the actions of CO dehydrogenase (CODH) and hydrogenase. Y19 requires O₂ for fast growth, but its H₂ production activity is significantly inhibited by O₂. In the present study, the effect of O₂ on the activities of CODH and hydrogenase was investigated quantitatively in both whole cells and broken cells, based on CO-dependent or methyl viologen (MV)-dependent H₂ production in addition to CO-dependent MV reduction. In crude cell extracts, CODH activity was mostly found in the soluble fraction. Inactivation of CODH and hydrogenase activities by O₂ followed the first-order decay kinetics, and the dependence of the rate constants on O₂ partial pressure could be expressed by the Michaelis-Menten equation. In whole cells, the maximum deactivation rate constants ($k_{d,max}$) of hydrogenase and CODH were quite similar: $0.07 \pm 0.03 \text{ min}^{-1}$ and $0.10 \pm 0.04 \text{ min}^{-1}$, respectively. However, the first-order rate constant ($k_{d,max}/K_s$) of CODH ($0.25 \text{ min}^{-1} \text{ atm}^{-1}$) at low O₂ partial pressures was about 3-fold higher than that of the hydrogenase, since the half-saturation constant (K_s) of CODH was about half of that of hydrogenase. In broken cells, both enzymes became significantly more sensitive to O₂ compared to the unbroken cells, while $k_{d,max}/K_s$ increased 37-fold for hydrogenase and 6.7-fold for CODH. When whole cells were incubated under anaerobic conditions after being exposed to air for 1 h, hydrogenase activity was recovered more than 90% in 2 h suggesting that the deactivation of hydrogenase by O₂ was reversible. On the contrary, CODH activity was not recovered once deactivated by O₂, and the only way to recover the activity was to synthesize new CODH. This study indicates that O₂ sensitivity of H₂ production activity of *Citrobacter* sp.

Y19 is an important drawback as in other H₂-producing bacteria.

Key words: *Citrobacter* sp. Y19, CODH, hydrogenase, oxygen sensitivity

H₂ is a clean, recyclable, and an efficient energy carrier. It has a high potential as a major fuel for fuel-cell powered vehicle. Currently, H₂ is mainly produced from a steam reforming of hydrocarbons, however, it will be substituted by a more environment-friendly biological process in the future [16, 20]. The microorganisms producing H₂ obtain the reducing power for their H₂-producing enzymes from various external sources such as CO, sugars, or light. Among them, the CO-dependent H₂ production occurs by the following water-gas shift reaction [13, 14]:



The deactivation of hydrogenase by O₂ has been reported in many H₂-producing bacteria including photosynthetic algae, *Cyanobacteria* [11, 16]. The inactivation is caused by denaturation of the enzyme active site by oxygen free radicals or the loss of catalytic activity by the change in redox state [1, 16]. CO-dependent H₂-producing bacteria are mostly strict-anaerobic or photosynthetic, and they are also known to be O₂-sensitive. Two enzymes are involved in the CO-linked H₂ production: a CODH (carbon monoxide dehydrogenase) oxidizes CO to CO₂ with the production of reducing power, and a hydrogenase reduces protons to H₂ by using the electrons donated from CODH. It is known that, by O₂, not only the activities of these enzymes are inhibited, but their expression is also repressed at the gene level [4]. However, individual O₂ dependence of CODH and hydrogenase has not been studied from the engineering

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point of view and, furthermore, no quantitative results have yet been reported.

Since the inactivation of hydrogenases by O₂ is a serious problem in development of H₂ production processes, many attempts have been made to avoid it. In a case of photoautotrophic process where O₂ is generated from water-splitting by photosystem II, various mechanical, chemical, and enzymatic methods have been suggested [11, 15]. Immobilization of *C. pasteurianum* has been reported to increase the stability of its hydrogenase to heat and O₂ [16]. However, these methods are economically not feasible at the present time due to high cost. Recently, Maness *et al.* [19] reported the isolation and characterization of an O₂-tolerant strain, *Rubrivivax gelatinosus*. The hydrogenase of this bacterium, linked to CO oxidation, had a long half-life of 21 h in air (21% O₂) and, furthermore, could function partially in the presence of O₂ [19].

Recently, a new chemoheterotrophic bacterium *Citrobacter* sp. Y19 was isolated [13, 14]. It can produce H₂ from fermentation of various sugars or from CO by water-gas shift reaction. With the CO-linked activity, Y19 differs from previously known strict anaerobes in that it grows fast under aerobic conditions and, on the other hand, produces H₂ under anaerobic conditions. Therefore, a two-stage cultivation that separates cell growth and H₂ production has been suggested as a desirable process. H₂ production activity of Y19 was also inhibited by O₂, but the individual sensitivity of CODH and hydrogenase has not been investigated.

The objective of this study was to quantitatively investigate the O₂ sensitivity of CODH and hydrogenase of Y19. Individual enzymatic activities were measured, based on CO-dependent or methyl viologen (MV)-dependent H₂ production along with CO-dependent MV reduction. Inactivation of hydrogenase and CODH was measured in unbroken whole cells and broken cells at various O₂ partial pressures, and the kinetic parameters were determined. Furthermore, reactivation or restoration of the enzymatic activities in O₂-inactivated whole cells and broken cells was studied.

MATERIALS AND METHODS

Cell Growth and Preparation of Crude Cell Extracts

Citrobacter sp. Y19 was grown in a serum bottle (total volume, 165 ml) on mineral salt medium [13] supplemented with 3 g yeast extract l⁻¹ and 5 g sucrose l⁻¹. Y19 was cultivated for 12 h under air/CO (95:5, v/v), which was replenished once at 6 h. After the cell growth, the culture bottle was completely deprived of O₂ by Ar purging and added with 20% CO. The bottle was further incubated for 24 h for induction of H₂ production activity. Detailed methods for cell growth and activity induction were described previously [12, 14].

Active cells were washed twice with an ice-cold phosphate buffer (pH 7.0, 100 mM). Cells were disrupted by using a bead beater (Fastprep FP120, Qbiogene Inc., U.S.A.) at a speed of 6.0 for 20 s twice with 10 s intervals. The conditions for cell breakage were determined to give the maximum CODH activity in a broken-cell suspension (see below). All procedures except for centrifugation were conducted in an anaerobic chamber (Bactron 1.5, Sheldon Manufacturing Inc., U.S.A.). Broken cells were centrifuged at 10,000 ×g and 4°C for 10 min to remove unbroken cells and large cell debris, and the supernatant was further centrifuged at 38,000 ×g and 4°C for 1 h to separate the particulate fraction from the soluble fraction [7, 21]. Particulate fraction was resuspended in the same phosphate buffer. Protein contents were assayed by the Bradford method (Protein assay kit, Bio-Rad Laboratories, U.S.A.) [3]. The broken cells and crude enzyme extracts were stored in sample vials at 4°C before use.

Deactivation by O₂ and Reversibility Experiments

For studying quantitative deactivation kinetics, whole cells and broken cells in a phosphate buffer (pH 7.0, 100 mM) were incubated at 30°C under different O₂ partial pressures (0–60%, v/v). Every 10 min, samples (2 ml) were taken into separate vials (8 ml) where the enzymatic activities were measured. Before use, the vials were purged with Ar gas, and 5 μl of 1 M sodium dithionite (SDT) was added to minimize the effect of O₂ carried over with the sample solutions. It was confirmed beforehand that the trace amount of SDT did not affect the assays for hydrogenase or CODH activities.

The reversibility of the activities of O₂-exposed hydrogenase and CODH was investigated by incubating both inactivated whole cells and broken cells under anaerobic conditions. After being exposed to air (21% O₂, v/v) for 1 h, the cells were incubated under 100% Ar or Ar/CO mixture (80:20, v/v). Since mechanical shear can affect the enzymatic activity in broken cells, two different methods, purging the Ar gas directly into the liquid solution and indirectly into the headspace, were attempted and compared. The effect of chloramphenicol (50 μM), a transcriptional inhibitor, was also studied in order to elucidate whether the reactivation of whole cell was induced by the restoration of deactivated enzyme or the synthesis of new enzymes.

Activity Assay

CO-dependent H₂ production activity of whole cells were assayed as described previously [14]. CODH activity was determined by the reduction of CO-dependent MV as follows [5, 6]. The 990 μl of 3[*N*-morpholino]propanesulfonic acid (MOPS; pH 7.5, 100 mM) containing 15 mM of MV and 1 mM of EDTA were introduced into a 10 mm quartz cuvette with a stopper which was maintained at 30°C by constant-temperature chamber. The buffer solution was

bubbled with pure CO for 5 min, and 10 µl of cell suspension or prepared enzyme solution (0.6–0.8 mg protein ml⁻¹) was added to start the reaction. The reduction of MV ($\epsilon_{578} = 9.7 \text{ mM}^{-1} \text{ cm}^{-1}$) was monitored at 578 nm for 20 min by a spectrophotometer (Lambda 20, Perkin-Elmer Inc., U.S.A.) [6, 9]. The absorbance increased linearly, and the activity was calculated from the slope of the absorbance change. Hydrogenase activity was determined by measuring the amount of H₂ produced with the reduced MV as an electron donor [5, 10]. Five-hundred µl of cell suspension or enzyme solution (0.6–0.8 mg protein ml⁻¹) containing 2.5 mM of MV and 200 mM of MOPS (pH 7.0) were introduced into an anaerobic serum vial (8 ml) and the head-space was replaced by purging Ar. The reaction was initiated by injecting an excess amount of 1 M SDT to become 50 mM. The total volume of liquid in the vial was 2 ml. The reaction mixture was incubated at 30°C in a reciprocally-shaking water bath (180 strokes min⁻¹) for 1 h, and the amount of H₂ produced was measured by a gas chromatograph (DS6200, Donam Instruments Inc., Korea) equipped with a thermal conductivity detector [5, 12, 23].

RESULTS AND DISCUSSION

Location and Activities of Hydrogenase and CODH

Table 1 shows the hydrogenase and CODH activities in whole cells and various fractions of crude cell extracts. Hydrogenase activity in a whole cell was 0.015 µmole H₂ min⁻¹ mg protein⁻¹, while the CODH activity in a whole cell was 0.030 µmole CO min⁻¹ mg protein⁻¹. Hydrogenase and CODH activities of the broken cells are significantly higher than those of the whole cells, indicating that the transfer of the reaction substrates through the intact cell wall could be an important barrier for the reactions. The higher CODH activity suggests that the hydrogenase activity might be the rate-limiting step for the CO-dependent H₂ production in Y19. This would be beneficial by enabling the cells to rapidly remove the intracellular CO, which is toxic to many cellular metabolisms. It should be noted that the specific CODH activity of Y19 broken cells (0.60 µmole CO min⁻¹ mg protein⁻¹) was similar to that of unpurified Ni-deficient apo enzyme of *R. rubrum* [5, 8], and that the specific hydrogenase activity (0.090 µmole H₂ min⁻¹ mg protein⁻¹) was about twice as high as that of *R. rubrum*

(0.050) or *E. coli* (0.047) [2, 16]. This confirms that Y19 is a highly active biocatalyst for water-gas shift reaction [13].

Table 1 also shows the cellular localization of CODH and hydrogenase activities in Y19. After centrifugation at 38,000 ×g, most CODH activity was found in the soluble fraction, indicating that CODH is a cytoplasmic protein, as reported with *R. rubrum* [6]. The specific activity of CODH in the soluble fraction was approximately 2.80 µmole CO min⁻¹ mg protein⁻¹, which was almost 5 times higher than that in broken cells. In the case of hydrogenase, no activity was found in the supernatant when the broken cell suspension was centrifuged at 10,000 ×g to remove unbroken cells and large cell debris. Consequently, no activity was found in either soluble fraction or particulate fraction following high-speed centrifugation. This observation, along with the fact that hydrogenase activity in broken cells was much higher than that of unbroken cells, suggests that most hydrogenase activity resides on cell debris in broken cells which are removed by the low-speed centrifugation. We also noticed that the cell breakage in this experiment was not complete, as evidenced by a large loss in protein content after low-speed centrifugation, and that hydrogenase enzyme molecules were not fully released from the subcellular compartment where they are located. Nevertheless, considering the appearance of high CODH activity in the 38,000 ×g fraction and a large increment of hydrogenase activity after cell breakage, some fractions of hydrogenase enzyme molecules must have been released during the cell breakage; however, their activity has been fully lost during the subsequent treatment, probably due to a high susceptibility of the hydrogenase to shear stress (see Fig. 3b). Hydrogenase activity in the cell-free system is important for its purification and characterization, but no further efforts were made in the present study.

Degradation of Hydrogenase and CODH Activities by Exposure to O₂

Figure 1 shows the deactivation of unbroken whole-cells and broken cells upon exposure to O₂. Both hydrogenase and CODH were very sensitive to O₂, and more than 50% of their activities were lost within 10 to 30 min when O₂ partial pressure was 17% (v/v). The deactivation rate increased with increasing O₂ partial pressure, as indicated by the increased slope. Compared to the unbroken cells, the enzymes of the broken cells were more sensitive to O₂.

Table 1. Distribution of CODH and hydrogenase activity in cell-free extract of *Citrobacter* sp. Y19.

	Whole cells	Broken cells	Supernatant at 10,000 ×g	Fractionation at 38,000 ×g	
				Soluble fraction	Particulate fraction
Protein content (µg ml ⁻¹)	620	600	210	50	160
Hydrogenase activity (µmole H ₂ min ⁻¹ mg protein ⁻¹)	0.015	0.090	0.0	0.0	0.0
CODH activity (µmole CO min ⁻¹ mg protein ⁻¹)	0.030	0.60	0.71	2.80	0.10

^aPrepared by centrifuging broken-cell suspension at 10,000 ×g to remove the unbroken cells and large cell debris.

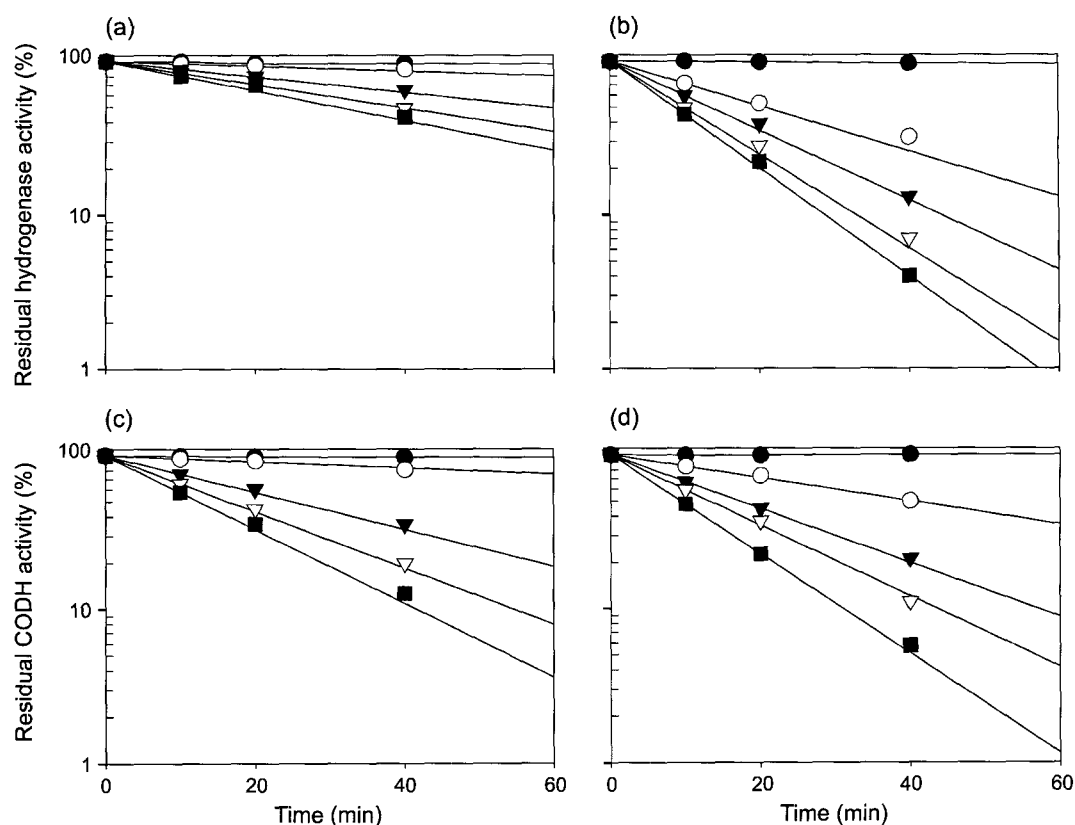


Fig. 1. Effect of O_2 partial pressure (% v/v) on (a) hydrogenase of whole cells, (b) hydrogenase of broken cells, (c) CODH of whole cells, and (d) CODH of broken cells.

Symbols: -●-, 0%; -○-, 5.0%; -▼-, 17.0%; -▽-, 27.0%; -■-, 60.0%.

The rate of activity loss followed the 1st order decay kinetics regardless of O_2 partial pressure.

$$-\frac{de_a}{dt} = r_d = k_d e_a \quad (2)$$

where e_a represents active enzyme concentration ($\mu\text{g ml}^{-1}$) or relative activity (%), and k_d represents deactivation rate constant (min^{-1}). The rate constant k_d was determined from the slope of Fig. 1 and followed the Monod-type kinetics.

$$k_d = \frac{k_{d,\max} P_{O_2}}{K_s + P_{O_2}} \quad (3)$$

where $k_{d,\max}$ represents maximum deactivation rate constant of the loss of activity upon exposure to O_2 (min^{-1}); K_s , half-

saturation constant (atm), and P_{O_2} , oxygen partial pressure (atm).

Table 2 summarized the kinetic parameters related with O_2 deactivation. In the case of the whole cell, the maximum deactivation rate of CODH was about 50% higher than that of hydrogenase. However, the 1st order activity loss rate ($k_{d,\max}/K_s$) of CODH at low O_2 partial pressures was about 3 times higher than that of hydrogenase, since K_s value of CODH was approximately half of that of hydrogenase. As comparison, kinetic parameters of O_2 deactivation of the CO-dependent H_2 production activity in a whole cell are also given. The $k_{d,\max}/K_s$ of CO-dependent H_2 production activity was 0.17, which was higher than that of hydrogenase but lower than that of CODH. After the cell breakage, O_2

Table 2. Kinetic parameters of deactivation of hydrogenase and CODH by O_2 ^a.

Type of exposure to O_2	Enzyme	$k_{d,\max}$ (min^{-1})	K_s (atm)	$k_{d,\max}/K_s$
Whole cell	Hydrogenase	0.07 ± 0.03	0.83 ± 0.10	0.08
	CODH	0.10 ± 0.04	0.41 ± 0.08	0.25
Broken cell	Hydrogenase	0.23 ± 0.06	0.08 ± 0.02	3.01
	CODH	0.42 ± 0.10	0.25 ± 0.03	1.68
Whole cell	Overall CO-dependent H_2 production activity	0.03 ± 0.01	0.16 ± 0.03	0.17

^aAssays were run in duplicate and averaged.

sensitivity of both hydrogenase and CODH greatly increased, as evidenced by 3–4 times higher $k_{d, \max}$ and 2–10 times lower K_s . This result suggests that the presence of cell membrane contributes to stabilizing CODH as well as hydrogenase, and the stabilization is related to a slower O₂ transfer in intact cells. Alternatively, O₂ scavenger systems such as superoxide dismutase (SOD) and catalase could play some important roles. The oxygen scavenger system is known to exist in facultative anaerobes such as *Citrobacter* sp. [22], but not in strict anaerobes.

Reactivation of Hydrogenase and CODH Under Anaerobic Conditions

In order to investigate whether the inactivation of hydrogenase and CODH by O₂ was reversible or not, the cells were exposed to air for 1 h and then incubated under anaerobic

condition. Figure 2 shows the results on the CO-dependent H₂ production activity in whole-cell suspension, while Fig. 3 shows the results on both hydrogenase and CODH activities in a whole-cell or broken-cell suspension. To prevent the cell growth during the experiment, 100 mM phosphate buffer at pH 7.0 was used as a suspending medium.

When the whole-cell suspension was exposed to air for 1 h, about 80% of the CO-dependent H₂ production activity was destroyed. When the inactivated cells were incubated under Ar/CO (80:20, v/v) mixture, the activity began to recover slowly after 1 h. However, the cells incubated with chloramphenicol, which is a transcriptional inhibitor, did not show any recovery. Cell density did not change for both cases. These results suggest that the reactivation during the anaerobic incubation is due to synthesis of new enzymes rather than reactivation of the enzymes present before the O₂ exposure.

Figure 3 shows the changes in hydrogenase and CODH activities during inactivation and subsequent reactivation processes. Forty % of hydrogenase activity in whole cells was lost and 80% in broken cells, when exposed to air for 1 h (Figs. 3a and 3b). When the inactivated cells were transferred to an anaerobic condition (100% Ar+chloramphenicol), reactivation was observed for both cells. In the case of the whole cells, 90% of the initial activity was recovered in 2 h, whereas the recovery was hardly detectable in the case of the broken cells, when Ar was bubbled through the broken-cell suspension to develop the anaerobic condition. When Ar was purged through the headspace instead, about 25% of the original activity was recovered in 2 h. These results indicate that the inhibition of hydrogenase by O₂ is reversible, although the enzyme is highly sensitive to shear stress. Reversible characteristics of hydrogenases have been reported with other strains [16, 18]. Figure 3(c) and 3(d) show the change in CODH activity. After 1 h exposure to air, CODH activity of the whole cells and broken cells decreased by 90% and 80%, respectively. Incubation of the inactivated cell suspensions under anaerobic condition (100% Ar) in the presence of chloramphenicol did not yield any reactivation differently from the case of hydrogenase. These results indicate that inactivation of CODH by O₂ is irreversible.

Reactivation of CO-dependent H₂ production requires both CODH and hydrogenase activities. Since CO-dependent H₂ production activity in whole cells was recovered during the incubation in Ar/CO (80:20, v/v) mixture (Fig. 2) but CODH activity was not recovered even after incubation in 100% Ar in the presence of chloramphenicol (Figs. 3c and 3d), the effect of CO and chloramphenicol on reactivation of the enzymatic activities were further investigated (Table 3). CODH activity in whole cells was recovered only, when CO was present but chloramphenicol was not. If chloramphenicol was present or CO was absent, CODH

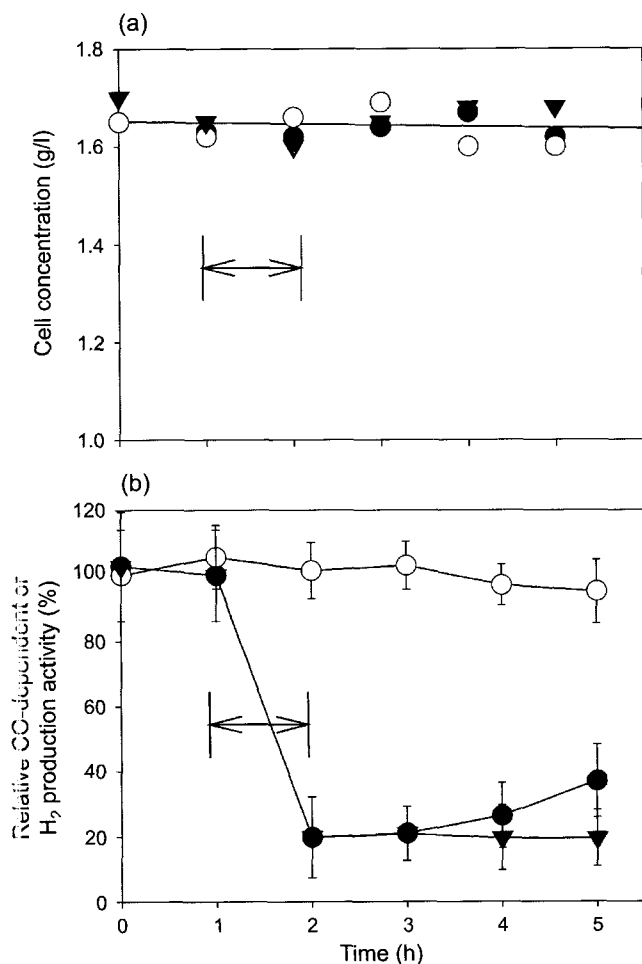


Fig. 2. Effect of transcription inhibitor (chloramphenicol) on (a) cell concentration, and (b) CO-dependent H₂ production activity of *Citrobacter* sp. Y19 upon exposure to air and reactivation by a subsequent anaerobic incubation.

Arrow represents the exposure period in full air. Symbols: ○, No exposure (control); ●, Exposure to air without chloramphenicol; ▼, Exposure to air with chloramphenicol.

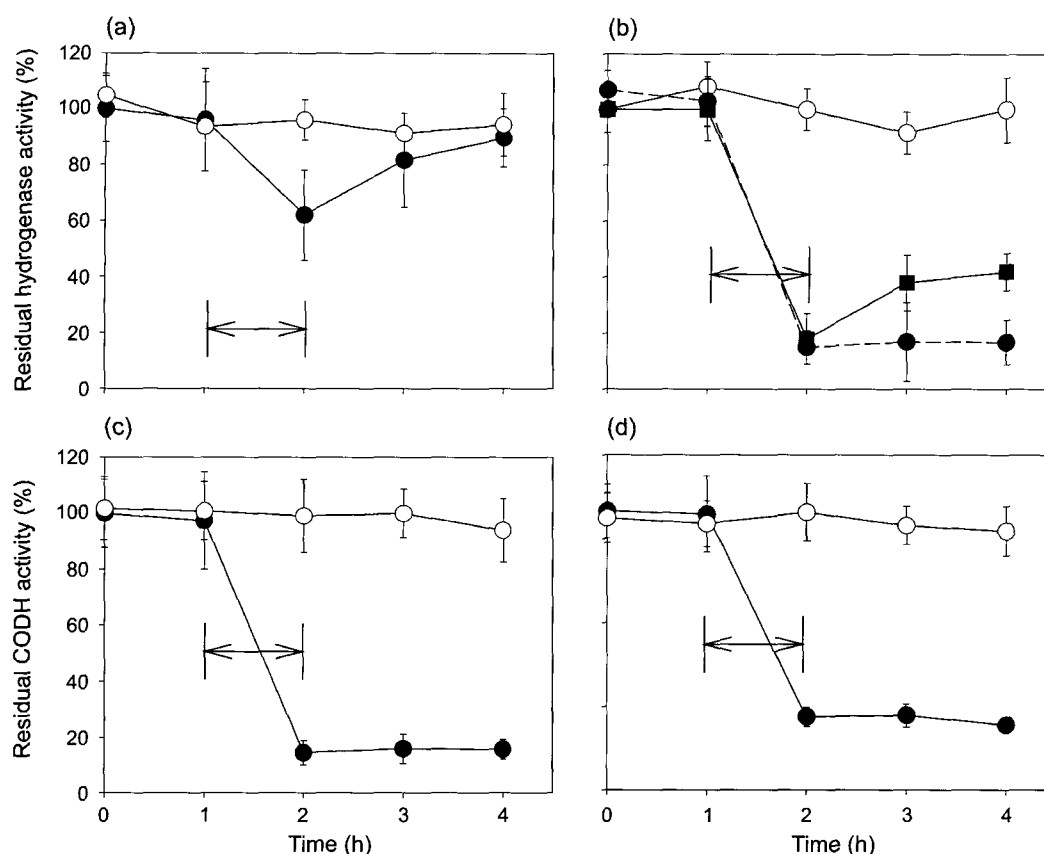


Fig. 3. Deactivation of H_2 production activity of Y19 upon exposure to air and reactivation by a subsequent anaerobic incubation. Arrow represents the exposure period in full air. (a) Hydrogenase of whole cells, (b) hydrogenase of broken cells, (c) CODH of whole cells, and (d) CODH of broken cells. Symbols: \circ -, No exposure (control); \bullet -, Exposure to air and a subsequent anaerobic incubation on 100% Ar. For anaerobic conditions O_2 was removed by bubbling Ar in reaction mixture except for the one case with (b) indicated by symbol \blacksquare where Ar was supplied to the headspace of reaction vial.

activity was not recovered by the anaerobic incubation. On the contrary, hydrogenase activity was not affected by the presence of chloramphenicol or CO. These results indicate that, once Y19 is exposed to O_2 and its CO-dependent activity is lost, the synthesis of new CODH is essential to recover the whole-cell H_2 production activity. CO as an inducer seems to promote the expression of CODH at gene level. Furthermore, since the reactivation of CODH occurs in a buffer solution which does not support the cell growth, *de novo* pathway seems to contribute to the synthesis of new enzymes.

The results from Figs. 1-3 and Table 3 indicate that both hydrogenase and CODH activities of Y19 are greatly inhibited by O_2 , but their inhibition modes are quite different. Because of irreversibility, O_2 inhibition of CODH might be more problematic than that of hydrogenase. However, it should be noted that Y19 has some advantages over strict anaerobes in recovering from O_2 inactivation. Y19 is a facultative anaerobe, and can aerobically grow very fast, when switched from an anaerobic condition [13]. This means that, although H_2 production

Table 3. Recovery of H_2 production activities in *Citrobacter* sp. Y19 after O_2 exposure^a.

Conditions	Hydrogenase ^b		CODH ^b		CO-dependent H_2 production in whole-cell suspension ^b
	Whole cell	Broken cell	Whole cell	Broken cell	
100% Ar+Chloramphenicol	+	+	-	-	-
100% Ar-Chloramphenicol	+	+	-	-	-
Ar/CO (80:20, v/v)+Chloramphenicol	ND ^c	ND ^c	-	-	-
Ar/CO (80:20, v/v)-Chloramphenicol	ND ^c	ND ^c	+	-	+

^aCells were incubated in 100 mM phosphate buffer (pH 7.0) that does not support cell growth.

^b(+) represents recovery of activity, while (-) represents no recovery.

^cNot determined.

activity may be lost by accidentally incorporating O₂ into the H₂ production process, O₂ can be depleted quickly from the fermentation broth, and both CODH and CO-dependent H₂ production activity could be recovered at a high rate under anaerobic condition. In the present study, we focused our effort on reversibility of enzymatic activities and used 100 mM phosphate buffer. If nutrient broth is used, the reactivation process can be accelerated, owing to the rapid cell growth. Lee *et al.* [17] have reported some supportive results with the facultative bacterium *Rhodospirillum rubrum* P4. The CO-dependent H₂ production activity in this strain which had been deactivated by O₂, could be successfully reactivated under oxygen-free condition by adding yeast extract and sucrose to the fermentation broth.

CONCLUSION

In *Citrobacter* sp. Y19, the enzyme activities related with CO-dependent H₂ production were severely inhibited by O₂. The rate of activity loss followed the 1st order decay kinetics, and its dependence on O₂ partial pressure could be expressed by the Michaelis-Menten kinetic equation. Hydrogenase was less sensitive to O₂ than CODH, and the inhibition was reversible. The inactivation of CODH by O₂ was irreversible and, once Y19 was exposed to O₂, the synthesis of new CODH was required for Y19 to recover the CO-dependent H₂ activity.

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NOMENCLATURE

Ar	: argon
CO	: carbon monoxide
MOPS	: 3[<i>N</i> -morpholino]propanesulfonic acid
MV	: methyl viologen
SDT	: sodium dithionite
e	: active enzyme concentration ($\mu\text{g ml}^{-1}$) or relative activity (%)
r_d	: volumetric rate of deactivation ($\mu\text{g ml}^{-1} \text{min}^{-1}$)
k_1	: 1 st order deactivation rate constant of the loss of activity upon exposure to O ₂ (min^{-1})
$k_{1,\text{max}}$: maximum deactivation rate constant of the loss of activity upon exposure to O ₂ (min^{-1})
K_s	: half-saturation constant for deactivation by O ₂ (atm)
P_{O_2}	: O ₂ partial pressure in gas phase (atm)

REFERENCES

- Adams, M. M. W. 1990. The structure and mechanism of iron-hydrogenases. *Biochim. Biophys. Acta* **1020**: 115–145.
- Adams, M. M. W. and D. O. Hall. 1979. Purification of the membrane-bound hydrogenase of *Escherichia coli*. *Biochem. J.* **183**: 11–22.
- Bae, E.-A., M. J. Han, M.-J. Song, and D.-H. Kim. 2002. Purification of rotavirus infection-inhibitory protein from *Bifidobacterium breve* K-110. *J. Microbiol. Biotechnol.* **12**: 553–556.
- Bonam, D., L. Lehman, G. P. Roberts, and P. W. Ludden. 1989. Regulation of carbon monoxide dehydrogenase and hydrogenase in *Rhodospirillum rubrum*: Effect of CO and oxygen on synthesis and activity. *J. Bacteriol.* **171**: 3102–3107.
- Bonam, D., M. C. McKenna, P. J. Stephens, and P. W. Ludden. 1988. Nickel-deficient carbon monoxide dehydrogenase from *Rhodospirillum rubrum*: *In vivo* and *in vitro* activation by exogenous nickel. *Proc. Natl. Acad. Sci. USA* **85**: 31–35.
- Bonam, D., S. A. Murrell, and P. W. Ludden. 1984. Carbon monoxide dehydrogenase from *Rhodospirillum rubrum*. *J. Bacteriol.* **159**: 693–699.
- Botes, A. L. 1999. Affinity purification and characterization of a yeast epoxide hydrolase. *Biotechnol. Lett.* **21**: 511–517.
- Ensign, S. A., M. J. Campbell, and P. W. Ludden. 1990. Activation of the nickel-deficient carbon monoxide dehydrogenase from *Rhodospirillum rubrum*: Kinetic characterization and reductant requirement. *Biochemistry* **29**: 2162–2168.
- Ensign, S. A., M. R. Hyman, and P. W. Ludden. 1989. Nickel-specific, slow-binding inhibition of carbon monoxide dehydrogenase from *Rhodospirillum rubrum* by cyanide. *Biochemistry* **28**: 4973–4979.
- Ensign, S. A. and P. W. Ludden. 1991. Characterization of the CO oxidation/H₂ evolution system of *Rhodospirillum rubrum*. *J. Biol. Chem.* **266**: 18395–18403.
- Ghirardi, M. L., S. Kosourov, and M. Seibert. 2001. Cyclic photobiological algal H₂-production, pp. 1–10. *In: Proceedings of the 2001 DOE Hydrogen Program Review*. Department of Energy, Washington, D.C., U.S.A.
- Jung, G. Y., H. O. Jung, J. R. Kim, Y. Ahn, and S. Park. 1999. Isolation and characterization of *Rhodospirillum rubrum* P4 which utilizes CO with the production of H₂. *Biotechnol. Lett.* **21**: 525–529.
- Jung, G. Y., J. R. Kim, H. O. Jung, J. Y. Park, and S. Park. 1999. A new chemoheterotrophic bacterium catalyzing water-gas shift reaction. *Biotechnol. Lett.* **21**: 869–873.
- Jung, G. Y., J. R. Kim, J. Y. Park, and S. Park. 2002. Hydrogen production by a new chemoheterotrophic bacterium *Citrobacter* sp. Y19. *Int. J. Hydrogen Energy* **27**: 601–610.
- Kim, N.-J. and C.-G. Lee. 2001. A theoretical consideration on oxygen production rate in microalgal cultures. *Biotechnol. Bioprocess Eng.* **6**: 352–358.
- Kondratieva, E. N. and I. N. Gogotov. 1983. Production of molecular hydrogen in microorganisms. *Adv. Biochem. Eng. Biotechnol.* **28**: 139–190.

17. Lee, T. H., J. Y. Park, and S. Park. 2002. Growth of *Rhodospseudomonas palustris* P4 under phototrophic and non-phototrophic conditions and its CO-dependent H₂ production. *Biotechnol. Lett.* **24**: 91–96.
18. Maness, P.-C., S. Smolinski, A. C. Dillon, M. J. Heben, and P. F. Weaver. 2002. Characterization of the oxygen tolerance of a hydrogenase linked to a carbon monoxide oxidation pathway in *Rubrivivax gelatinosus*. *Appl. Environ. Microbiol.* **68**: 2633–2636.
19. Maness, P.-C. and P. F. Weaver. 2001. Biological H₂ from fuel gases and from water, pp. 67–76. *In: Proceedings of the 2001 DOE Hydrogen Program Review*. Department of Energy, Washington, D.C., U.S.A.
20. Nandi, R. and S. Sengupta. 1998. Microbial production of hydrogen: An overview. *Crit. Rev. Microbiol.* **24**: 61–84.
21. Park, S., M. L. Hanna, R. T. Taylor, and M. W. Droege. 1991. Batch cultivation of *Methylosinus trichosporium* OB3b. I: Production of soluble methane monooxygenase. *Biotechnol. Bioeng.* **38**: 423–433.
22. Stanier, R. Y., J. L. Ingraham, M. L. Wheelis, and P. R. Painter. 1986. *The Microbial World*, pp. 210–212. 5th ed. Prentice-Hall, Englewood Cliffs, New Jersey, U.S.A.
23. Woo, K., H. Yang, and W. Lim. 2002. Effects of polyurethane as support material for the methanogenic digester of a two-stage anaerobic wastewater digestion system. *J. Microbiol. Biotechnol.* **12**: 14–17.